



## Engineering Photocatalytic TiO<sub>2</sub>/CuWO<sub>4</sub> Coatings: The Synergistic Effect of Oxidants on Heavy Metal Remediation

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### ABSTRACT

A highly active TiO<sub>2</sub>/CuWO<sub>4</sub> heterostructure coating for Cr<sup>6+</sup> photoreduction was developed through PEO and hydrothermal post-treatment. Characterizations such as FESEM, GXR, AFM and wettability, revealed that nano-sized CuWO<sub>4</sub> integration transforms the morphology, producing a hierarchical, microporous base with uniformly distributed particles and a super-hydrophilic, rough surface for improved accessibility. Oxidant screening revealed that both radical (SO<sub>4</sub><sup>•-</sup>, HO<sup>•</sup>) and non-radical species are critical to the mechanism. Peroxydisulfate (PDS) achieved the highest synergy (synergistic factor= 0.9) via sulfate radical generation, significantly outperforming peroxymonosulfate (PMS) and the ineffective H<sub>2</sub>O<sub>2</sub>. This study proposes a dual-pathway mechanism and introduces a durable, scalable photocatalytic coating solution for environmental cleanup.

**Keywords:** Cr photoreduction, Oxidants, plasma electrolytic oxidation, hydrothermal, TiO<sub>2</sub>/CuWO<sub>4</sub> Coatings.

### 1. Introduction

Rapid urban and industrial expansion has significantly intensified water contamination through the persistent discharge of hazardous materials [1-3]. A particularly severe global environmental concern is the presence of hexavalent chromium Cr<sup>6+</sup> in water supplies, which ranks among the most perilous pollutants. To address this, numerous conventional and advanced techniques for Cr<sup>6+</sup> removal from wastewater have been established, each with its own set of benefits and drawbacks [4,5]. In the last ten years, semiconductor-based photocatalysis has emerged as a promising strategy for environmental cleanup,

especially in treating wastewater. This approach is further enhanced by the inclusion of oxidants, which are crucial for degrading aqueous pollutants more effectively [6]. On the other hand, oxidizing agents such as peroxymonosulfate (PMS), peroxydisulfate (PDS), and hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>) boost photocatalytic performance by facilitating the creation of reactive oxygen species (ROS) and improving the separation of photogenerated charges [7,8]. Titanium dioxide (TiO<sub>2</sub>) is a widely studied photocatalyst, valued for its cost-effectiveness, chemical stability, potent oxidizing ability, non-toxic nature, and biocompatibility, establishing it as a standard material in environmental and energy

technologies [9]. Nonetheless, its widespread use is hindered by a large bandgap that restricts light absorption to ultraviolet wavelengths and a tendency for rapid recombination of electron-hole pairs, which diminishes quantum yield [10,11]. To overcome these shortcomings, strategies such as heterojunction engineering have been adopted to make  $\text{TiO}_2$  responsive to visible light and to improve the separation of charge carriers [12-14]. Copper tungstate ( $\text{CuWO}_4$ ), an n-type semiconductor, has gained interest due to its promising electronic and optical properties for photocatalysis. While photocatalysts in powder form provide high reactivity, their real-world utility is hampered by difficulties in retrieval, low reusability, and a tendency for particles to clump together, which blocks active sites and impedes light. Consequently, research has shifted towards immobilized photocatalytic coatings as a more viable solution. Depositing the photocatalyst as a thin film onto a support material offers multiple benefits: it increases stability and reusability, allows for optimized light absorption through controlled thickness, prevents particle aggregation, and simplifies the process of separating the catalyst from the purified water [15]. Plasma Electrolytic Oxidation (PEO) is noted as a particularly effective method for producing  $\text{TiO}_2$ -based photocatalytic coatings, as it can generate porous, strongly adhered, and customizable surfaces [16,17]. Recent improvements in PEO coatings involve both pre- and post-treatment methods. Pre-treatments condition the substrate to enhance coating quality, whereas post-treatments, such as hydrothermal processing, alter the coating's structure to create nanostructures that significantly increase photocatalytic activity [12,18,19].

To better understand the photocatalytic reduction mechanism of chromium, this study used various scavengers and oxidants, as detailed earlier, to analyze the behavior of the hydrothermally post-treated PEO-synthesized  $\text{TiO}_2/\text{CuWO}_4$  photocatalyst.

## 2. Experimental

### 2.1. Chemicals and substrates

A Ti substrate with dimensions of  $20 \times 15 \times 1$  mm was used; its chemical composition has been reported elsewhere [20]. Potassium hydroxide (KOH), sodium phosphate dodecahydrate ( $\text{Na}_3\text{PO}_4 \cdot 12\text{H}_2\text{O}$ ), sodium tungstate ( $\text{Na}_2\text{WO}_4$ ) and copper(II) acetate ( $\text{Cu}(\text{CH}_3\text{COO})_2$ ) were purchased from Merck Co. (Germany). Additionally, potassium chromate ( $\text{K}_2\text{CrO}_4$ ) as pollutant, scavengers, and oxidants such as methanol ( $\text{CH}_3\text{OH}$ ), sodium pyruvate ( $\text{C}_3\text{H}_3\text{NaO}_3$ ), (tert-butanol ( $\text{C}_4\text{H}_{10}\text{O}$ ), peroxymonosulfate ( $\text{KH}_2\text{O}_5$ , PMS), hydrogen peroxide ( $\text{H}_2\text{O}_2$ ), and peroxydisulfate ( $\text{K}_2\text{S}_2\text{O}_8$ , PDS) procured from Sigma-Aldrich (USA).

### 2.2. Production of the coatings

Prior to the PEO process, the titanium sheets were prepared by sequential grinding with abrasive papers, followed by ultrasonic cleaning in distilled water and acetone for five minutes each, and finally air-drying. The PEO was performed using a pulsed DC power supply. The Ti substrates, acting as the anode, were fully immersed in an electrolyte solution contained in a stainless-steel vessel that served as the cathode. A water-cooling system was used to maintain the electrolyte temperature below  $40^\circ\text{C}$  during the process. The specific PEO parameters were selected based on our previous work [21], (electrical parameters: duty cycle=80, frequency=1000 Hz, time=10 min, current density=  $12 \text{ A/dm}^2$ , electrolyte=  $5 \text{ gr/L Na}_3\text{PO}_4$  and  $4 \text{ gr/L KOH}$ ) and the resulting sample is designated as "T."

The hydrothermal post-treatment, adapted from Hang et al. [22] with modifications, was employed to grow crystalline  $\text{CuWO}_4$  nanoparticles on the  $\text{TiO}_2$  coating. Briefly,  $0.3 \text{ M Na}_2\text{WO}_4$  and  $0.3 \text{ M Cu}(\text{CH}_3\text{COO})_2$  were dissolved in  $40 \text{ mL}$  of deionized water under magnetic stirring for one hour, forming a sky-blue suspension. This solution was transferred to a Teflon-lined autoclave, where the T sample was placed on a holder. The sealed autoclave was then heated at  $180^\circ\text{C}$  for 24 hours. The final product is labeled as "TC."

### 2.3. Characterization of the coatings

A suite of characterization techniques was employed to analyze the coatings. Field-emission scanning electron microscopy (FE-SEM) revealed the morphology and elemental distribution. Surface wettability was assessed via static water contact angle measurements, while X-ray diffraction (XRD) with  $\text{CuK}\alpha$  radiation, including grazing incidence mode, determined the crystalline structure. Atomic force microscopy (AFM) mapped the surface topography and measured roughness. The photocatalytic activity (PA) of the coatings was evaluated by measuring the reduction of hexavalent chromium ( $\text{Cr}^{6+}$ ) under visible light at room temperature. Prior to illumination, the coatings (with a surface area of  $3 \text{ cm}^2$ ) were immersed in  $30 \text{ mL}$  of a  $5 \text{ ppm Cr}^{6+}$  solution and stirred in the dark for 30 minutes to establish adsorption-desorption equilibrium. Subsequently, the solution containing the samples was irradiated using a  $100 \text{ W}$  visible LED lamp. During the photocatalytic reaction,  $0.5 \text{ mL}$  aliquots were collected from the reactor at regular intervals from 1 to 6 hours. The concentration of  $\text{Cr}^{6+}$  was specifically determined by the diphenylcarbazide method [4]. For this test, a  $0.5 \text{ mL}$  sample was mixed with  $2 \text{ mL}$  of deionized water,  $0.04 \text{ mL}$  of  $\text{H}_2\text{SO}_4$  ( $10\% \text{ v/v}$ ), and a diphenylcarbazide solution ( $0.65\% \text{ w/w}$  in acetone). The absorbance of the resulting solution was measured at  $540 \text{ nm}$  using

a Teksan-lena SB-G100 spectrophotometer. The influence of oxidants was studied by adding 5 mM of  $\text{H}_2\text{O}_2$ , PMS ( $\text{KHSO}_5$ ), or PDS ( $\text{K}_2\text{S}_2\text{O}_8$ ). To probe the reaction mechanism, methanol and tert-butanol (TBA) at 0.01 M and sodium pyruvate (9.1 mM) acted as scavengers for hydroxyl, sulfate radicals and  $\text{H}_2\text{O}_2$ , respectively.

### 3. Result and discussion

As shown in Fig. 1, the TC and T coatings both possess the porous, sponge-like morphology inherent to the PEO fabrication process, which is caused by gas evolution and the rapid quenching of molten oxide [23]. The key morphological distinction is the successful incorporation of

well-dispersed Copper tungstate ( $\text{CuWO}_4$ ) nanoparticles within the porous network of the TC coating, achieved through hydrothermal modification.

Fig. 2 displays the grazing-angle XRD patterns, which confirm the successful hydrothermal modification. Both the T and TC coatings are primarily composed of anatase  $\text{TiO}_2$  (ICDD 00-071-1167), with titanium substrate peaks (ICDD 00-088-2321) visible due to the thin, porous oxide layer [24]. The defining feature of the TC coating's pattern is the presence of new peaks that match the reference for triclinic  $\text{CuWO}_4$  (ICDD 00-080-1918), conclusively identifying the product of the hydrothermal treatment as crystalline copper tungstate.

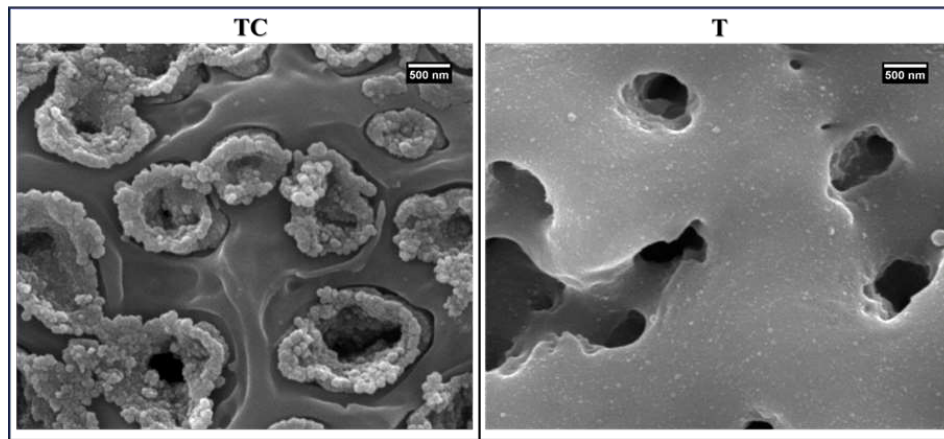


Fig. 1- FESEM micrographs of coatings [20].

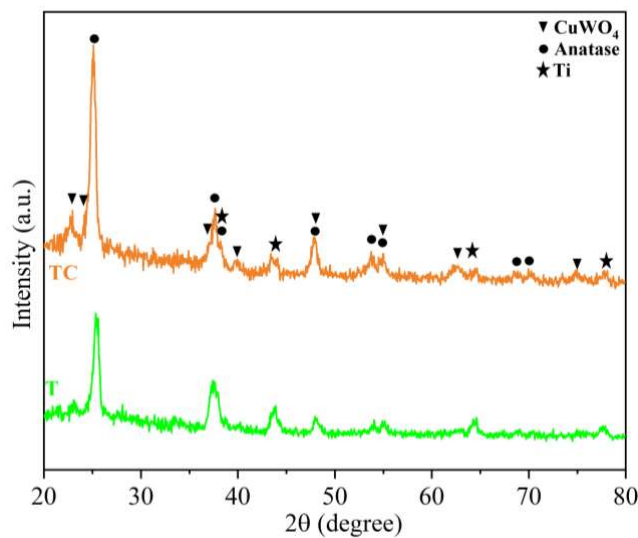


Fig. 2- GXRD patterns of T and TC coatings [20].

AFM topography analysis (Fig. 3) indicates that the hydrothermal process uniformly deposited  $\text{CuWO}_4$  particles on the coating, resulting in a substantial increase in average roughness ( $R_a$ ) from 31.75 nm to 75.94 nm.

As shown in Fig. 4, the hydrothermally modified TC coating displayed superhydrophilic behavior with an unmeasurable contact angle, a significant improvement over the  $85^\circ$  angle of the pristine T coating. This phenomenon is consistent with the established principle that surface roughness is a key determinant of wettability [25]. The increased roughness of the

TC coating, quantified by AFM, enhances water spreading by reducing interfacial tension.

The photoreduction efficiency of  $\text{Cr}^{6+}$  using various oxidants, including peroxymonosulfate (PMS), peroxydisulfate (PDS), and hydrogen peroxide ( $\text{H}_2\text{O}_2$ ) is presented in Fig. 5(a). As observed, the addition of PDS significantly enhanced the photoreduction process. This outcome aligns with mechanisms reported in prior studies [8], as a greater amount of PDS is converted into sulfate radicals  $\text{SO}_4^{\cdot-}$  under acidic conditions, such as the experimental pH of 5.5. Below are the chemical reactions for

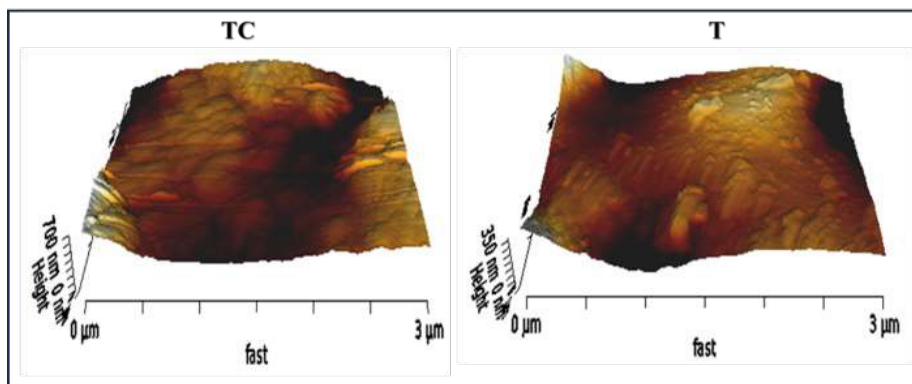


Fig. 3- AFM images (scan sizes of  $3 \times 3 \mu\text{m}$ ) for T and TC samples.

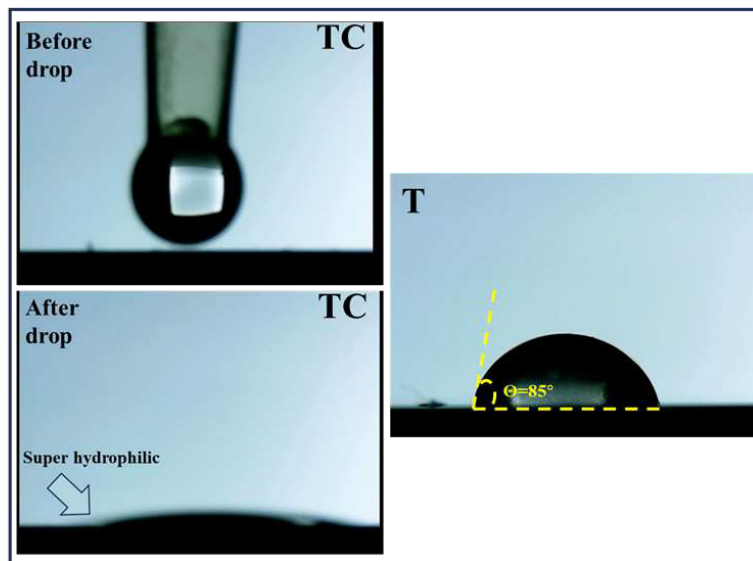
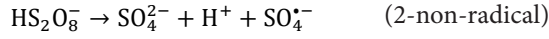
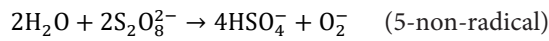


Fig. 4- Wettability test for TC and T samples.

both radical and non-radical pathways during PDS activation [26,27]:



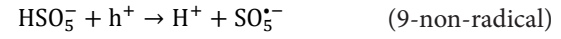
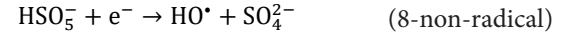
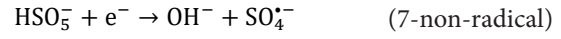
Additionally, the decomposition of persulfate generates hydrogen ions ( $\text{H}^+$ ), which contribute to the acidic environment of the reaction system (Eqs. (5,6)) [8]:



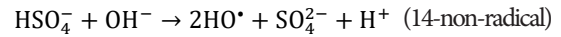
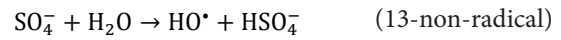
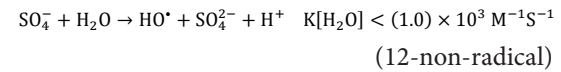
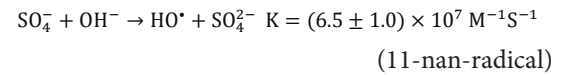
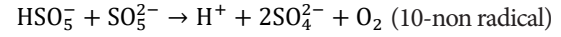
In the case of PMS in the photoreaction, the results closely resemble those of the previous oxidant. Given that the radical species generated by both oxidants are likely similar, methanol and tert-butanol were utilized as trapping agents to more precisely examine and identify the presence or participation of  $\text{HO}^\bullet$  and  $\text{SO}_4^{\bullet-}$ . As reported in the literature [8], the reaction rate constants of methanol and tert-butanol with hydroxyl radicals  $\text{HO}^\bullet$  are comparable, with ( $k_{\text{HO}^\bullet/\text{Methanol}} = 9.7 \times 10^8 \text{ M}^{-1}\text{s}^{-1}$  and  $k_{\text{HO}^\bullet/\text{Tert-butanol}} = 3.8\text{--}7.6 \times 10^8 \text{ M}^{-1}\text{s}^{-1}$ ). However, the kinetic constant describing the interaction of methanol with sulfate radicals  $\text{SO}_4^{\bullet-}$  is noticeably higher ( $1.6\text{--}7.7 \times 10^7 \text{ M}^{-1}\text{s}^{-1}$ ) compared to that of tert-butanol with  $\text{SO}_4^{\bullet-}$  ( $k = 4.0\text{--}9.1 \times 10^5 \text{ M}^{-1}\text{s}^{-1}$ ). This difference makes methanol a more effective trapping agent for  $\text{SO}_4^{\bullet-}$  than tert-butanol. Therefore, to assess the effect of  $\text{SO}_4^{\bullet-}$ , same concentration of both scavengers was used. As perceived in Fig. 5(c), the addition of methanol to the solution caused the  $\text{Cr}^{6+}$  photoreduction efficiency to decrease to 32%. In contrast, when tert-butanol was added, the efficiency increased to 74%. These results confirm the production of both sulfate radicals  $\text{SO}_4^{\bullet-}$  and hydroxyl radicals  $\text{HO}^\bullet$ , with  $\text{SO}_4^{\bullet-}$  representing a dominant part in the  $\text{Cr}^{6+}$  photoreduction process. The difference in inhibition behavior between the two scavengers is attributed to methanol's greater ability to scavenge sulfate radicals compared to tert-butanol. Moreover, the kinetic behavior of both scavengers was plotted in Fig. 5(d), validating previous results.

Similar to PDS, PMS activation also proceeds through both radical and non-radical mechanisms. As an oxidant, PMS could act as an electron acceptor in photoreduction reactions. In the non-radical mechanism, electrons transferred from the coating to PMS appear to generate  $\text{SO}_4^{\bullet-}$  and  $\text{HO}^\bullet$ ,

as described in Eqs. (7,8). Furthermore, the holes produced in the VB interact with PMS, leading to the formation of  $\text{SO}_5^{\bullet-}$  radical, as outlined in Eq. 9 [28,29]:

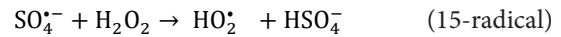


Meanwhile, the solution pH is an essential variable influencing the production process/rate and the distribution of  $\text{SO}_4^{\bullet-}$  species and hydroxy complexes on the surface of the catalyst [30]. Additionally,  $\text{OH}^-/\text{H}_2\text{O}$  can be relatively oxidized into hydroxyl radicals  $\text{HO}^\bullet$  by  $\text{SO}_4^{\bullet-}$  and/or  $\text{HSO}_5^-$  within the (3–9) pH range, as described in Eqs. (10–14).

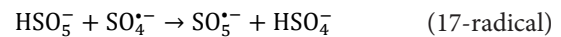
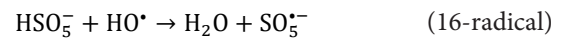


PMS may shift from non-radical mechanisms to radical ones upon activation. It releases  $\text{H}^+$  ions, which acidify the solution, thereby enhancing the oxidative capacity of  $\text{Cr}^{6+}$ . Based on these acidic circumstances, the redox potential of  $\text{Cr}^{6+}$  is approximately 1.10 V, while the redox potentials of superoxide radicals  $\text{O}_2^{\bullet-}$  and singlet oxygen  ${}^1\text{O}_2$  are about 0.89 V and 0.81 V, respectively [31].

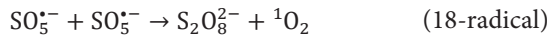
The recombination of  $\text{HO}^\bullet$  radical can lead to the formation of  $\text{H}_2\text{O}_2$  [32]. Subsequently, hydrogen peroxide  $\text{H}_2\text{O}_2$  interacts with sulfate radicals  $\text{SO}_4^{\bullet-}$  to produce hydroperoxyl radicals  $\text{HO}_2^\bullet$  (Eq. 15) [33].



Also, the radicals produced in Eqs. (7–9) lead to the formation of the  $\text{SO}_5^{\bullet-}$  radical, as outlined in Eqs. (16,17). Owing to their rapid reaction rate, the recombination of  $\text{SO}_5^{\bullet-}$  radicals happen swiftly, giving rise to singlet oxygen ( ${}^1\text{O}_2$ ) through an alternative pathway, as described in Eq. 18 [33].







The self-scavenging influence (Eq. 19) is not important as long as the concentration of  $\text{SO}_4^{\bullet-}$  stays low, since  $\text{SO}_4^{\bullet-}$  is rapidly consumed in oxidation reactions.



Based on the findings from the photocatalytic activation of PMS and PDS, a unified reaction pathway of  $\text{Cr}^{6+}$  photoreduction, with the TC coating serving as the activator under visible

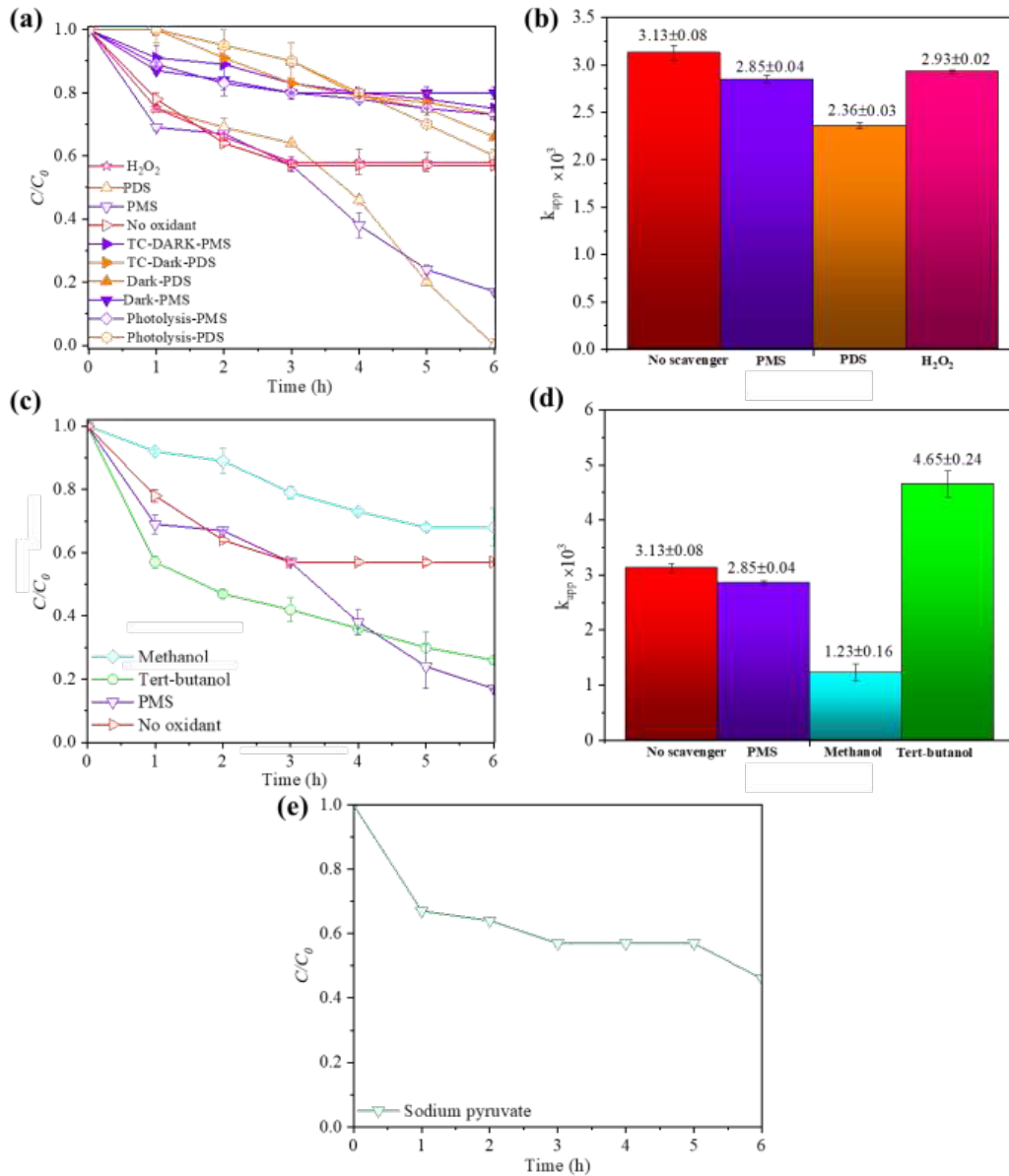


Fig. 5- Evaluation of the photocatalytic  $\text{Cr}^{6+}$  reduction performance using the TC coating under visible light, (a) Comparison of  $\text{Cr}^{6+}$  removal efficiency under dark and visible light conditions across different oxidants, (b) The corresponding apparent pseudo-first-order rate constants ( $k$ ), (c) The impact of radical scavengers, methanol (MeOH) and tert-butanol (TBA), on  $\text{Cr}^{6+}$  removal in the TC-PMS system, (d) The calculated reaction rate constants for the scavenger experiments and (e) sodium pyruvate scavenger for  $\text{H}_2\text{O}_2$ . Experimental conditions: initial  $\text{Cr}^{6+}$  concentration,  $[\text{Cr}]_0 = 5 \text{ mg/L}$ ; initial oxidant concentration,  $[\text{PMS}, \text{PDS}, \text{H}_2\text{O}_2]_0 = 5 \text{ mM}$ ; scavengers' concentration for PMS and  $\text{H}_2\text{O}_2$ , 0.01M, 9.1mM respectively.

light illumination, is proposed. Fig. 6, provides a schematic representation, encompassing relevant reactive oxygen species whose roles in  $\text{Cr}^{6+}$  photoreduction have been either confirmed or hypothesized. The radical and non-radical pathways are distinguished using two different colors, corresponding to the specific reactions involved. The tip of each arrow denotes the resulting product of the respective reaction sequence. The only special feature in Fig. 6 is the intersection marked with a plus symbol, which indicates the simultaneous presence of both reactive species at that point in the mechanism.

Finally, the influence of PMS and PDS activation mediated by the TC coating on the photoactivity rate constant of  $\text{Cr}^{6+}$  was compared, as seen in Fig. 5(b). Both the TC/PMS and TC/PDS systems demonstrated nearly similar  $\text{Cr}^{6+}$  reduction activity under dark and visible light circumstances. The interactive influence of the components contributing to the reaction was analyzed using rate constants, as detailed in our prior study [34]. Table 1 provides the synergy indices corresponding to PMS and PDS activation, together with the rate constants obtained for the TC coating. The synergy values for the TC/PMS/Vis and TC/PDS/Vis systems were calculated to be 0.60 and 0.90, respectively. These results highlight the significant advantage of using the TC catalyst

in PMS and PDS-enhanced  $\text{Cr}^{6+}$  photoreduction, achieving saturation in 6 h compared to the 3-hour saturation observed with the T sample alone.

$\text{H}_2\text{O}_2$  possesses a dual redox nature, enabling it to participate in both oxidation and reduction reactions. As an oxidant, it can accept electrons [ $E^0(\text{H}_2\text{O}_2/\text{H}_2\text{O}) = 1.77 \text{ V}$ ], while as a reductant it donates electrons [ $E^0(\text{O}_2/\text{H}_2\text{O}_2) = 0.68 \text{ V}$ ]. This dual functionality allows  $\text{H}_2\text{O}_2$  to drive the interconversion between  $\text{Cr}^{3+}$  and  $\text{Cr}^{6+}$  species. Specifically, the interplay of the  $\text{Cr}^{6+}/\text{Cr}^{3+}$  and  $\text{O}_2/\text{H}_2\text{O}_2$  redox pairs suggests that  $\text{H}_2\text{O}_2$  promotes the oxidation of  $\text{Cr}^{3+}$  to  $\text{Cr}^{6+}$  at alkaline pH ( $> 8$ ), whereas under acidic or near-neutral conditions it favors the reduction of  $\text{Cr}^{6+}$  to  $\text{Cr}^{3+}$  [35]. Although the solution pH was around 9, as could be seen in Fig. 5(a),  $\text{H}_2\text{O}_2$  acted neither as an oxidant nor a reductant. The neutral—or, in other words, ineffective—behavior of this oxidant was also confirmed using the sodium pyruvate scavenging test (Fig. 6(e)). Considering the small pH difference between the experimental conditions and the oxidation zone discussed above, it can be inferred that the likelihood of oxidation influencing chromium increases with the basicity of the solution. Moreover, as the system deviates further from the defined oxidation and reduction zones, the behavioral distinction between these regions becomes more pronounced.

Table. 1- Synergistic factor associated with PMS and PDS activation by the TC sample under visible illumination

Conditions	$k \times 10^3 \text{ (min}^{-1}\text{)}$	Synergistic factor
Photolysis	0.65 ( $\pm 0.01$ )	
Photolysis/PMS	1.21 ( $\pm 0.01$ )	
PMS/Dark	0.80 ( $\pm 0.09$ )	
PDS/Dark	0.90 ( $\pm 0.17$ )	-
Photolysis/PDS	0.60 ( $\pm 0.15$ )	
TC/Dark	0.75 ( $\pm 0.10$ )	
TC/Vis	3.13 ( $\pm 0.33$ )	
TC/PMS/Dark	0.96 ( $\pm 0.15$ )	0.6
TC/PMS/Vis	2.85 ( $\pm 0.04$ )	
TC/PDS/Dark	1.08 ( $\pm 0.26$ )	0.9
TC/PDS/Vis	2.36 ( $\pm 0.03$ )	

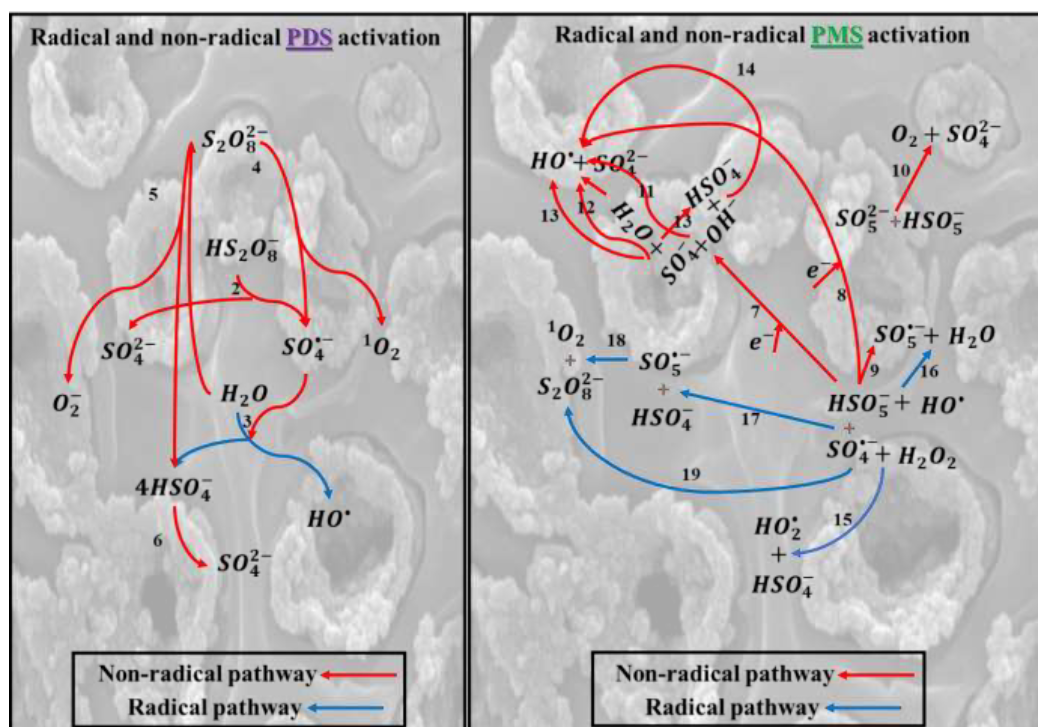


Fig. 6- The anticipated photocatalytic pathway of the TC coating under visible light exposure, incorporating PMS and PDS.

#### 4. Conclusion and future prospective

In summary, a hydrothermally synthesized  $\text{TiO}_2/\text{CuWO}_4$  coating demonstrated high efficacy for visible-light  $\text{Cr}^{6+}$  photoreduction via synergistic radical and non-radical mechanisms. Material analyses revealed that  $\text{CuWO}_4$  incorporation drastically increased surface roughness (100% increment) and imparted super hydrophilic character (from  $85^\circ$  to near zero degrees). The photocatalytic activity was governed by ( $\text{SO}_4^{\cdot-}$ , and  $\text{HO}^{\cdot}$  radicals), with PDS proving to be a more effective than PMS by 0.9 calculated synergistic factor compared to that of 0.6. It has to be mentioned that, ozone, periodate (and its associated iodate and periodate radicals), and percarbonate may also be considered in future research to determine the most appropriate oxidant for Cr photoreduction.

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